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**Nyota Minerals Limited ('Nyota' or the 'Company')**

**TULU KAPI METALLURGICAL TEST RESULTS**

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**HIGHLIGHTS**

- **Test work results demonstrate highly encouraging average gold recoveries from Tulu Kapi ore samples**
- **Recoveries in excess of 95% achieved**
- **Results will support prefeasibility level capital and operating cost estimates for a gold recovery plant at Tulu Kapi**
- **Results demonstrate the potential for high recoveries and low operating costs when Tulu Kapi commences production**

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Nyota Minerals Limited (AIM:NYO/ASX:NYO), which is focused on the exploration and development of gold and nickel projects in Africa, is pleased to announce highly encouraging results from the metallurgical test work program completed on samples from its Tulu Kapi gold project, Ethiopia, in January 2010.

Nyota Director, Dr Evan Kirby, selected samples totaling 277kg in weight for the metallurgical test work during a site visit to Tulu Kapi in December 2009. The samples were taken from diamond drill core from the exploration drilling that formed the basis for the maiden JORC resource estimate of 690,000 ounces. Samples were taken from both Lodes One and Two. The metallurgical test work was conducted at AMMTEC Laboratories in Perth, Australia.

The results are considered extremely encouraging and demonstrate the potential for high recoveries and low operating costs when Tulu Kapi commences production.

Melissa Sturgess, Nyota CEO, commented "we couldn't be more encouraged by these test results. The sample of about 300kg is significant and the testwork was done to prefeasibility standards in a world class laboratory, giving us a high level of confidence that when Tulu Kapi commences production we will be able to build a low cost processing plant to extract the gold from the ore."

## SUMMARISED RESULTS

TESTWORK DETAILS	RESULTS	
	Lode One	Lode Two
HEAD ANALYSIS		
Gold g/t	3.47	5.17
Silver g/t	1.55	4.69
Sulfur %	2.5	2.25
Silica %	61.7	57.3
COMMUNUTION PARAMETERS		
Bond Rod Mill Work Index (kWh/tonne)	17.4	19.1
Bond Ball Mill Work Index (kWh/tonne)	16.3	18.2
Bond Abrasion Index	0.50	0.58
CYANIDATION		
Gold dissolution % at grind P80 of 75 microns	98.1	98.6
Gold dissolution at grind P80 of 150 microns	95.1	96.2
BULK ROUGHER FROTH FLOTATION		
Gold recovery % at grind P80 of 75 microns	99.5	96.1
Gold recovery % at grind P80 of 150 microns	99.5	96.1

## DETAILS OF THE TEST WORK

The comminution test work used standard methods and equipment. Closing screen sizes of 1120 microns and 106 microns were used in the Bond Rod Mill and Ball Mill tests.

The cyanidation work comprised a series of monitored bottle-roll tests, each with duration 24 hours. Leaching conditions included a lime addition rate of 0.3 kg/t and cyanide solution strength of 0.050%. An oxygen atmosphere was used in the leaching bottles. No supplementary cyanide or lime additions were made during the leaches.

The bulk flotation tests were conducted on one kilogram portions of sample in a standard laboratory flotation cell. The duration of each float was 15 minutes. In all cases, the mass pull to concentrate was about 10% of the feed mass.

## SELECTION OF THE METALLURGICAL TESTWORK SAMPLES

All intersections shown on the geological sections were reviewed; a realistic mining width for each intersection was estimated and the value in g.m (g/t \* meters width) was calculated. Intersections with values less than 5 g.m were not considered for sampling.

Intersections with values greater than 5 g.m were then selected from the upper and lower lodes (Lode One and Lode Two respectively). The half core from these intersections was then sawn and portions of quarter core were taken for the composites. The average intersection widths and estimated average grades in Lodes One and Two composites were 11.1 m @ 3.1 g/t and 7.2 m @ 4.9 g/t respectively.

The intersections making up the Lode One and Lode Two composites are summarized below in Tables One and Two.

Table One  
Intersections Comprising the Lode One Composite

Section	Hole	From	To	Width (m)	Grade (g/t)	Value (g.m)	Actual Weight (kg)
160S	14	59	63.8	4.8	7.37	35	7
160S	14	93.77	98.2	4.43	2.91	13	6
80S	12	56.63	68.4	11.77	4.6	54	20.2
80S	10	31	48.7	17.7	5.37	95	23.5
80S	10	63.75	75.15	11.4	1.8	21	15.8
0	8	64.9	98.85	33.95	1.82	62	64
0	8	107	111.05	4.05	5.79	23	4.5
0	20	94.1	101.9	7.8	1.81	14	9
0	20	114	118.3	4.3	2.08	9	4.2

The total weight of the lode one composite was 154 kg.

Table Two  
Intersections Comprising the Lode Two Composite

Section	Hole	From	To	Width (m)	Grade (g/t)	Value (g.m)	Actual Wt (kg)
240S	25	187.7	192.56	4.86	8.95	43	5.2
160S	26	161	174	13	3.69	48	23
160S	17	137	141	4	4.68	19	4.2
80S	27	212	231.68	19.68	5.01	99	36
80S	10	201	203.82	2.82	9.24	26	2.6
0	8	215.61	242.62	27.01	1.74	47	25
0	20	201	205	4	11.26	45	4
0	20	215.19	217	1.81	3.06	6	1.9
0	20	245	247	2	5.02	10	2
80N	33	207	209.64	2.64	21.2	56	2.6
160N	6	150.12	154.63	4.51	7.08	32	4.5
160N	31	178	182.2	4.2	5.17	22	7
160N	31	212.7	215.4	2.7	3.8	10	5.0

The total weight of the lode two composite was 123 kg.

#### **PREFEASIBILITY STUDY USE OF THE TESTWORK RESULTS**

The test work results will be used to generate pre-feasibility level estimates of the capital and operating costs of gold recovery plants for Tulu Kapi. The comminution parameters will be used to specify crushing and grinding equipment and estimate wear parts consumption. The cyanidation and froth flotation results will be used to specify equipment requirements and estimate operating costs and gold recoveries.

Two alternative flow sheets will be considered. The first consists of crushing and grinding followed by conventional CIP gold recovery. This is the standard flow sheet used throughout the world where the ore is “free milling”, i.e. gold can be cyanide leached from finely ground ore.

An alternative flowsheet involving the production of a concentrate and then cyanidation of the concentrate will also be considered. This flowsheet has advantages in environmentally sensitive areas and has been implemented in a number of recent gold plants.

In the alternative, the ore is crushed and milled and then gold recovered to a concentrate

with a mass of less than 10% of the feed by means of gravity concentration and froth flotation. The non-toxic tailings from this process, comprising more than 90% of the mass of ore, can be stored in a simple tailings storage facility. Excess water can be discharged to the environment.

The concentrate is then subject to intensive cyanidation to recover the gold. Cyanide is recycled in the leach process and the tailings are detoxified to destroy any residual cyanide. The tailings from concentrate leaching are then either sold for the sulfur content, or stored in a secure impoundment.

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The technical exploration and mining information contained in this Announcement has been reviewed and approved by Dr Evan Kirby. Dr Kirby has sufficient experience which is relevant to the style of mineralisation and type of deposit under consideration and to the activity which he is undertaking to qualify as a Competent Person as defined in the 2004 Edition of the 'Australasian Code for Reporting of Exploration Results, Mineral Resources and Ore Reserves' and as a qualified person under the AIM Note for Mining, Oil and Gas Companies. Dr Kirby is a director of Nyota Minerals Limited and is a member of the Australasian Institute of Mining and metallurgy (Aus.I.M.M). Dr Kirby consents to the inclusion in this Announcement of such information in the form and context in which it appears.